

— 2003 IMF Review

# *Novel Modified Zeolites for Energy-Efficient Hydrocarbon Separations*

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Tina M. Nenoff, Mutlu Ulutagay-Kartin, Chris Cornelius,  
Thomas M. Anderson

*June 25, 2003*



# — Agenda

- Team Members
- Background
- Project
  - Description and Goals
  - Milestones
  - Funding
  - Benefits
- Technical
- Summary

# — Research Team

## *Sandia National Laboratories*

Tina M. Nenoff  
Mutlu Ulutagay-Kartin  
Chris Cornelius

## *Goodyear Chemical*

Jeff Goodwin  
Gary Gray

## *Nofsinger*

Tom Anderson  
Geoff Stephenson

*Synthesis  
Characterization*

*Pilot-Plant Testing*

*Process Modeling*

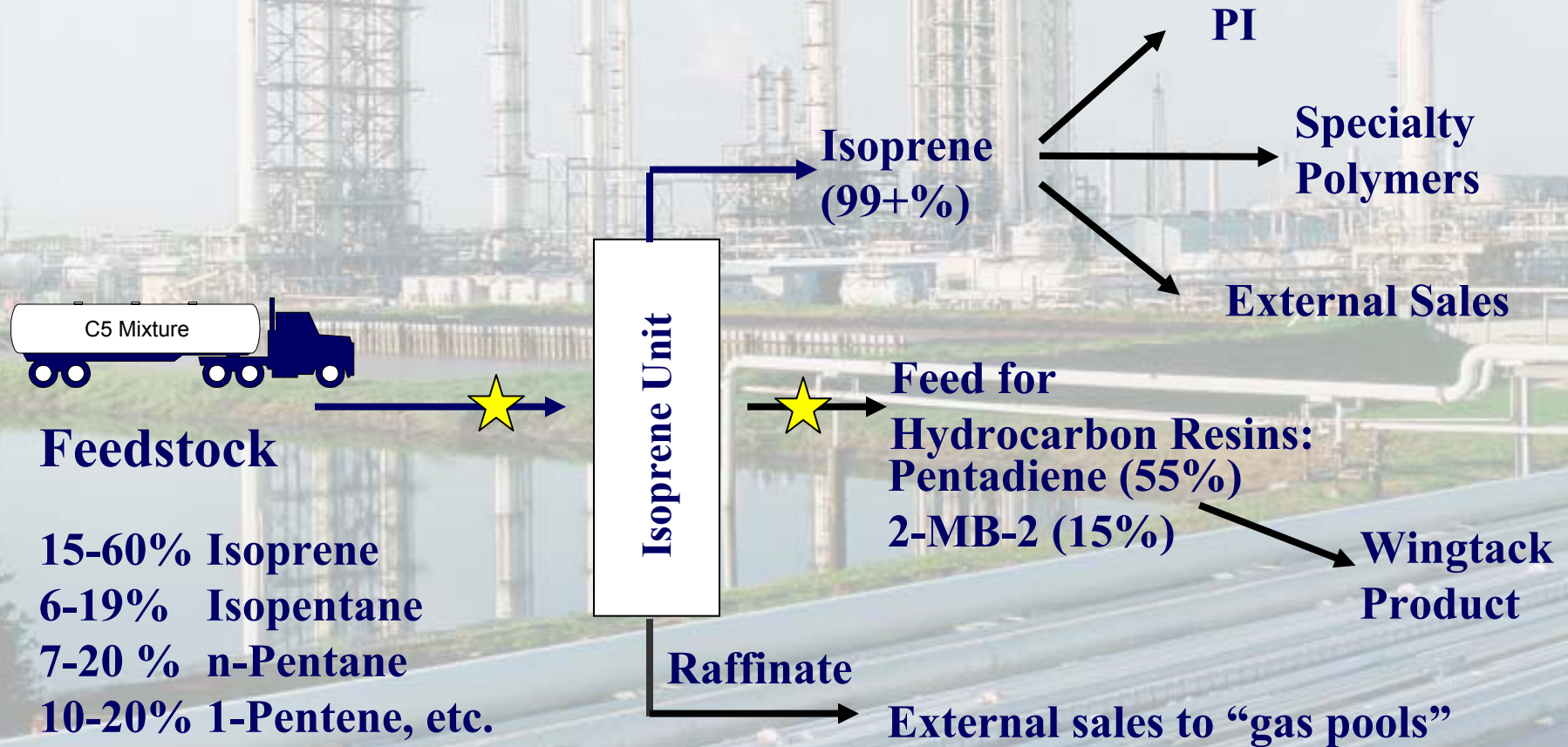


# —Background/Business Case

**Objective: Reduced Energy Consumption Using Membranes**



## Current Isoprene Monomer Technology



★ Potential Separation Location

# — DOE/IMF Project Description & Goals

## Description

### Create materials for Energy Efficient HC separations

- Scientific focus on surface modified zeolites
- Enrichment / separation of isoprene from C5 stream
- Separations to provide basis of application toward other energy-intensive C2-C5 separation processes

## Goals

- Develop new membrane materials or separation-based adsorbents via **modification of commercially-available zeolites**
- Establish zeolite structure-property models for this technology & others
- Decrease energy consumption in the chemical & petroleum industries by employing these new & improved materials

# —Goodyear and Sandia Project Milestones

## Milestones

**Yr1:** Zeolite Modification and testing; Go/No Go  
Initial Economic Analysis

**Yr2:** Selection of “best” modified zeolite through  
characterization and testing; large scale  
synthesis

**Yr3:** Pilot Plant testing, material modification;  
In-depth economic calculations;  
Engineering Analysis

## — DOE/OIT/IMF Project Funding

### *“Novel Modified Zeolites for Energy-Efficient Hydrocarbon Separations”*

#### *Collaborative Research*

*198K/yr* OIT/IMF “Direct to SNL”

*188K/yr* Goodyear “In-Kind”

*10K/yr* Nofsinger “In-Kind”

*\$1.2M / 3yr program (FY02-04)*

*50% “in-kind” industry funding,  
commenced 4/23/2002.*



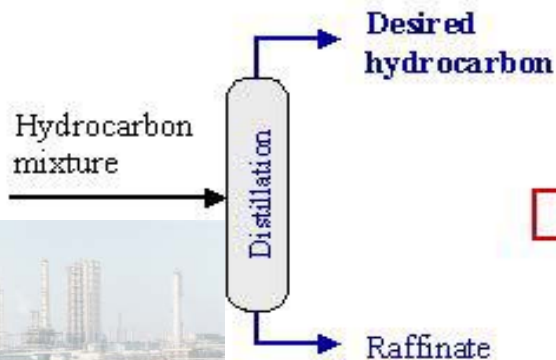
**Potential Benefits to Goodyear: Energy Savings**

**Need: Process Improvement for Isoprene Separation**

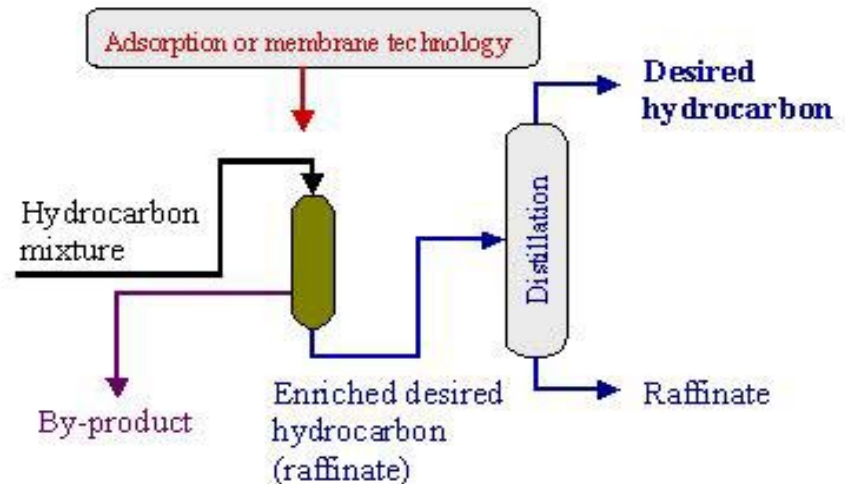
**Current Technology**

**Proposed Technology**  
Adsorption or Membrane Separation

**22% Reduction in Energy**



**NEW**



**Energy Intensive**

**Less Energy Intensive**



## — Potential Energy Benefits to U.S. Chemical Industry

- Goodyear is domestic leader in isoprene production (60%).
- Economic Modeling from Nofsinger shows 22% reduction in Energy of Isoprene Process Using modified Zeolites (membranes). Goodyear saves 1 trillion Btu/yr.
- Extrapolation to C<sub>2</sub>-C<sub>5</sub> industries predicts 64 Trillion BTU's savings

	Btu/yr Trillion	2002 Billion lbs	Btu/lb
Ethylene- C2	214	53	4,058
Propylene-C3	53	39	1,359
Butadiene-C4	21	4	5,366
Isoprene- C5	5	0.4	8,000+
Total	293		

**64 Trillion Btu's**

22 % Reduction

Source: CMAI - 2003

DOE/OIT Energy & Environ. Profile 2002



# — Technical Section: Previous Technology Review

- Current technology - energy intensive fractional and extractive distillation
- Past patent literature shows the use of activated carbon/mole sieves technology\* but does not have zeolite pore selectivity properties
- Other unmodified zeolite membranes rapidly deactivate from olefin & diolefin exposure

\* US Patent Nos. 4,570,029 Kulprathipanja, S. , UOP Inc.; 3,596,436 Dassese, P., Solvay & Cie.



# — Technical Section: Separations Methodology

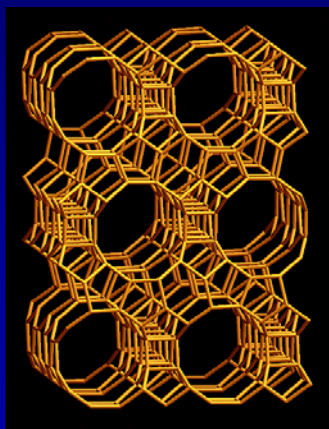
Sandia IP for Modified Zeolite Technology,  
combined leads to *enhanced* HC selectivity:

- 1) Molecular Sieving (pore size)**
- 2) Adsorption Modification  
(surface carbonization + acidity/reactivity)**
- 3) Deactivation Stabilized  
(high temp; multiple cycles)**



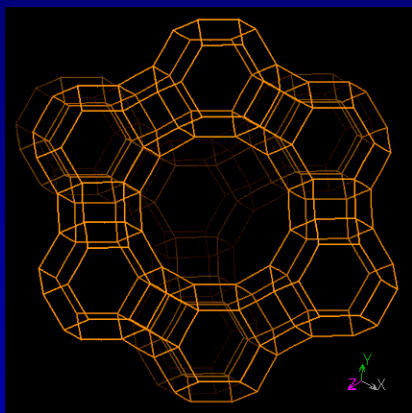
# —Technical Section - Zeolites for Separations

	Relative acidity	Pore diameter (Å)
<b>Zeolite <math>\beta</math></b>	<b>high</b>	<b>6.6 x 7.7, 5.6</b>
<b>Zeolite-Y</b>	<b>medium-high</b>	<b>7.4</b>
<b>Zeolite-L</b>	<b>low</b>	<b>7.1</b>
<b>ZSM-5</b>	<b>high</b>	<b>5.1 x 5.5</b>



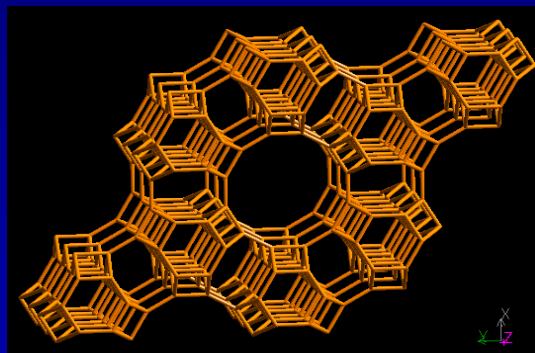
**Zeolite- $\beta$**

**12 MR (3-D)  
straight pores**



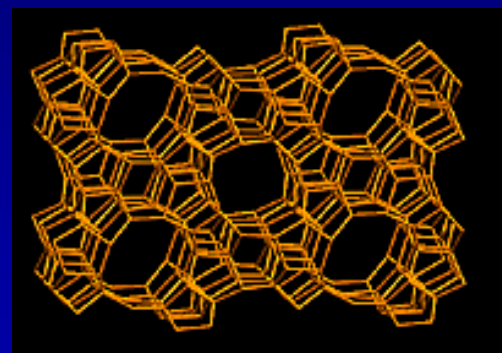
**Zeolite-Y**

**12 MR (3-D, cages)  
intersecting straight pores**



**Zeolite-L**

**12 MR (1-D)  
straight pores**



**ZSM-5**

**10 MR (3-D)  
Intersecting straight /  
sinusoidal pores**

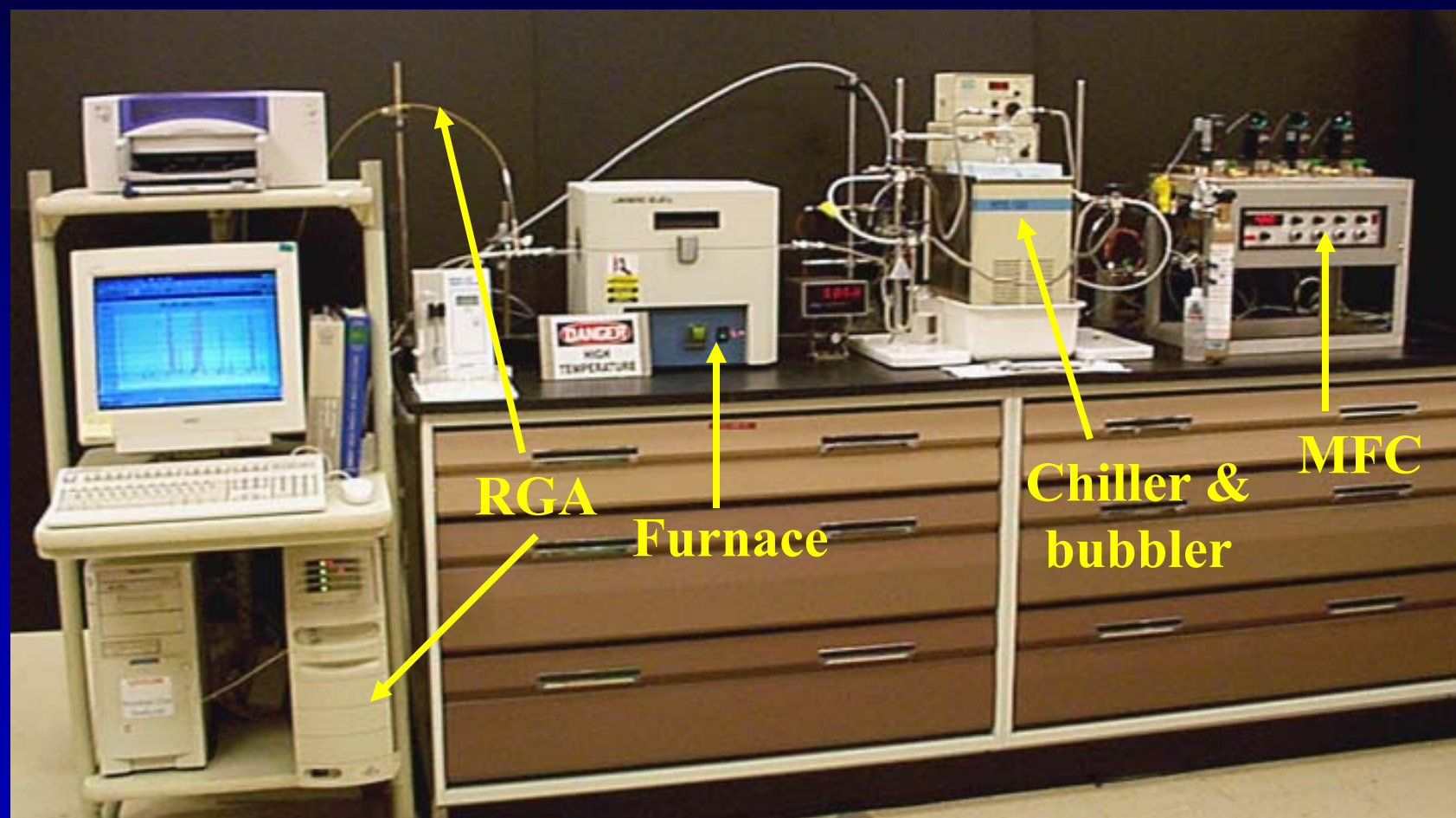


# —Technical Section - Zeolite Modification (Acid site deactivated & pore size modified)

- ***Activating Zeolite:*** The zeolites (crystalline molecular sieves) are regenerated at high temp to remove ancillary pore-blocking molecules.
- ***Bulk Carbonization:*** The regenerated zeolites are carbonized w/HC. hydrocarbon type/mixture, concentration, helium flow rate, exposure time, and temperature
- ***Temperature Programmed Desorption (TPD) Experiments:*** The effect of bulk carbonization on the adsorptivity of the zeolites is assessed with temperature-programmed desorption experiment.
- ***Separation Experiments:*** The carbonized zeolites are used for separation of a hydrocarbon from a hydrocarbon mixture.



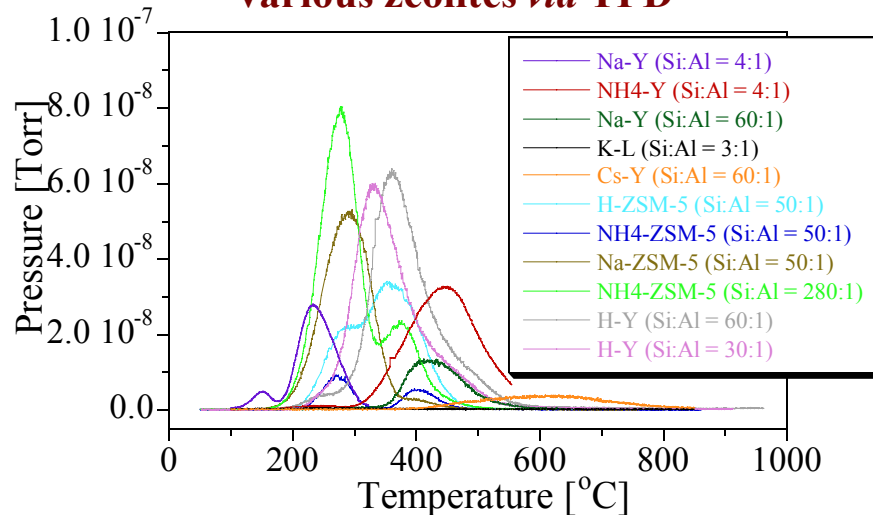
## — Technical Section : In-house Sandia Reactor



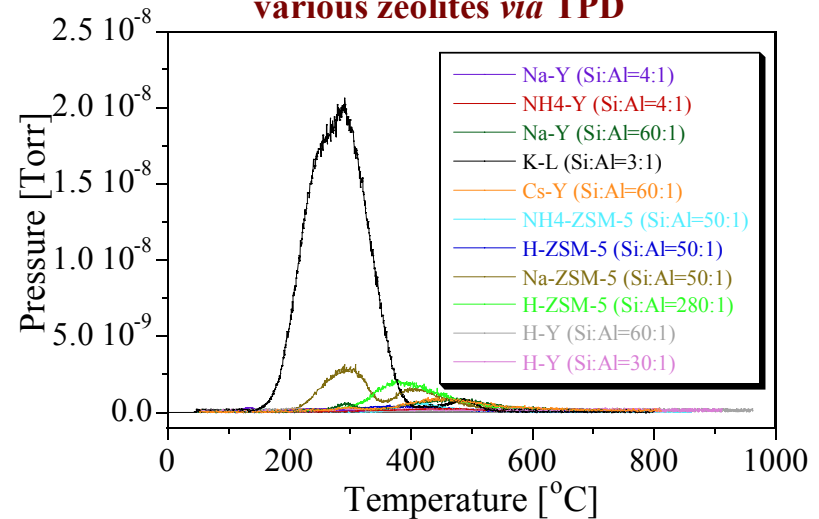
# — Technical Section : Surface Modification

- *TPD experiments show that surface modification occurs at the active sites of the interior pores.*
- *Zeolite Y have selective adsorption for n-Pentane but no adsorption for Isoprene*

**n-pentane desorption of various zeolites via TPD**



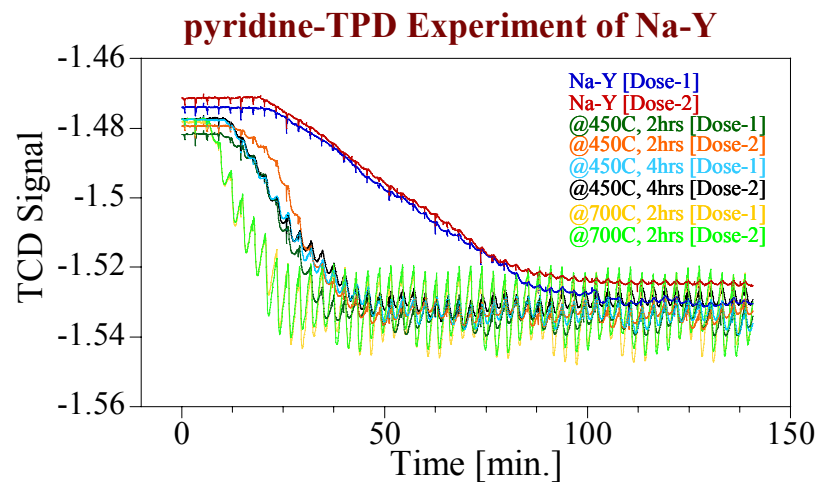
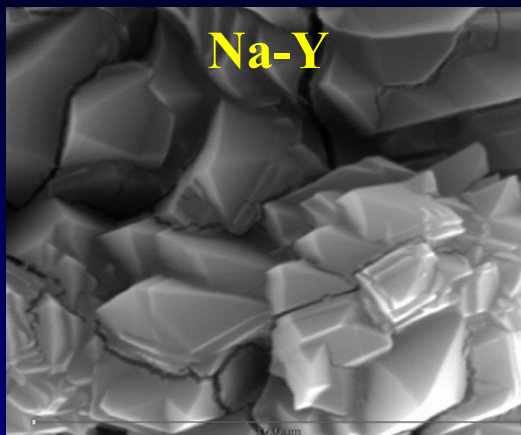
**isoprene desorption of various zeolites via TPD**



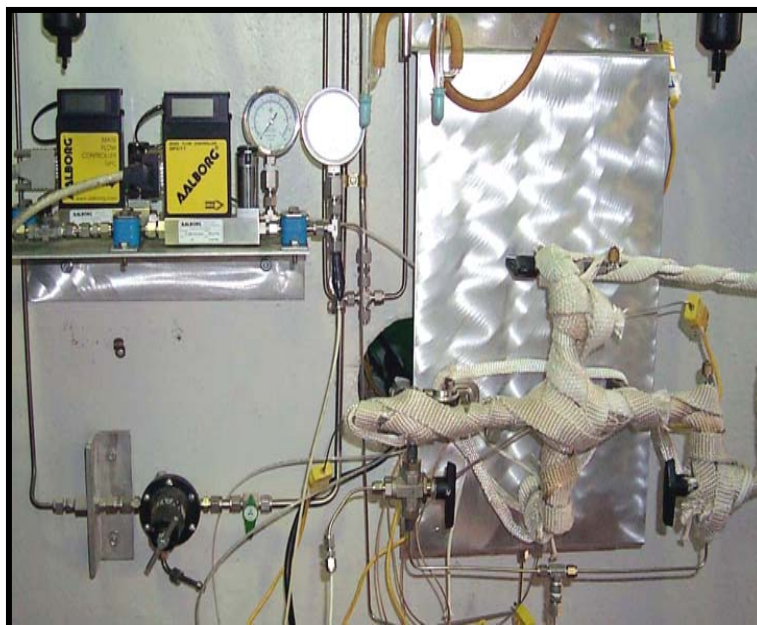
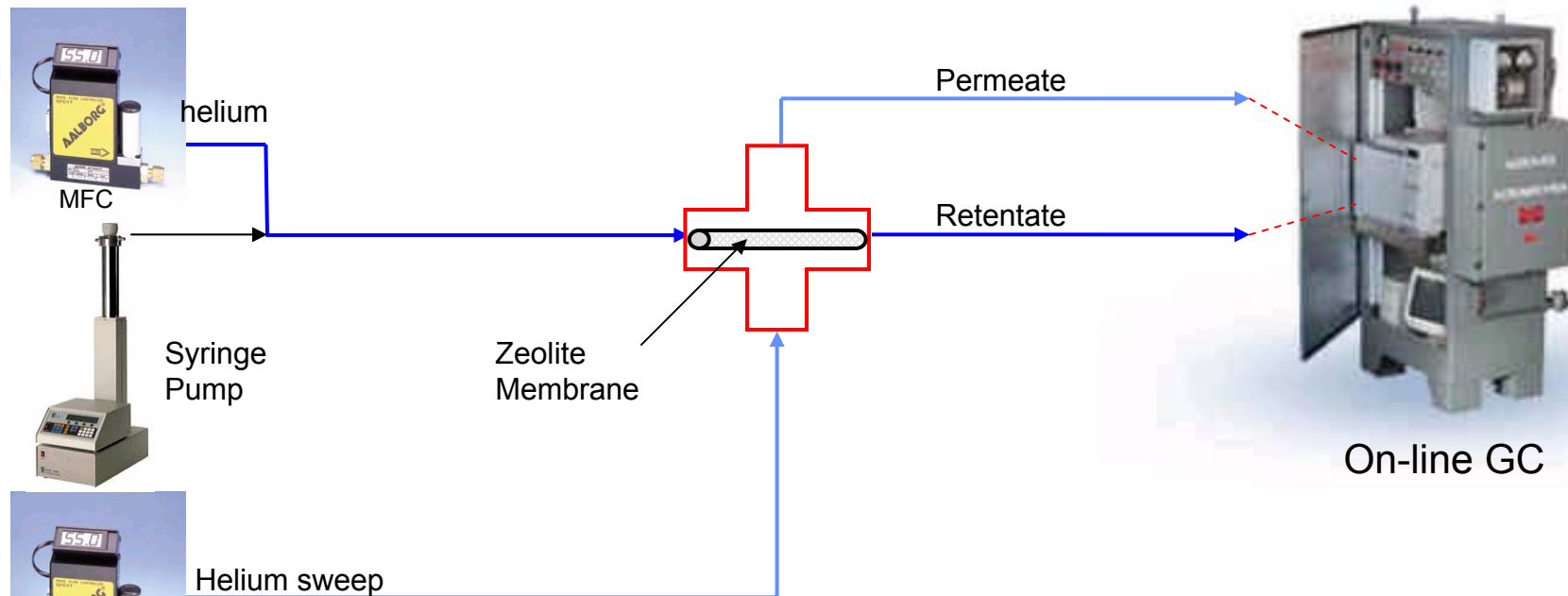


# — Technical Section : Characterization Methods

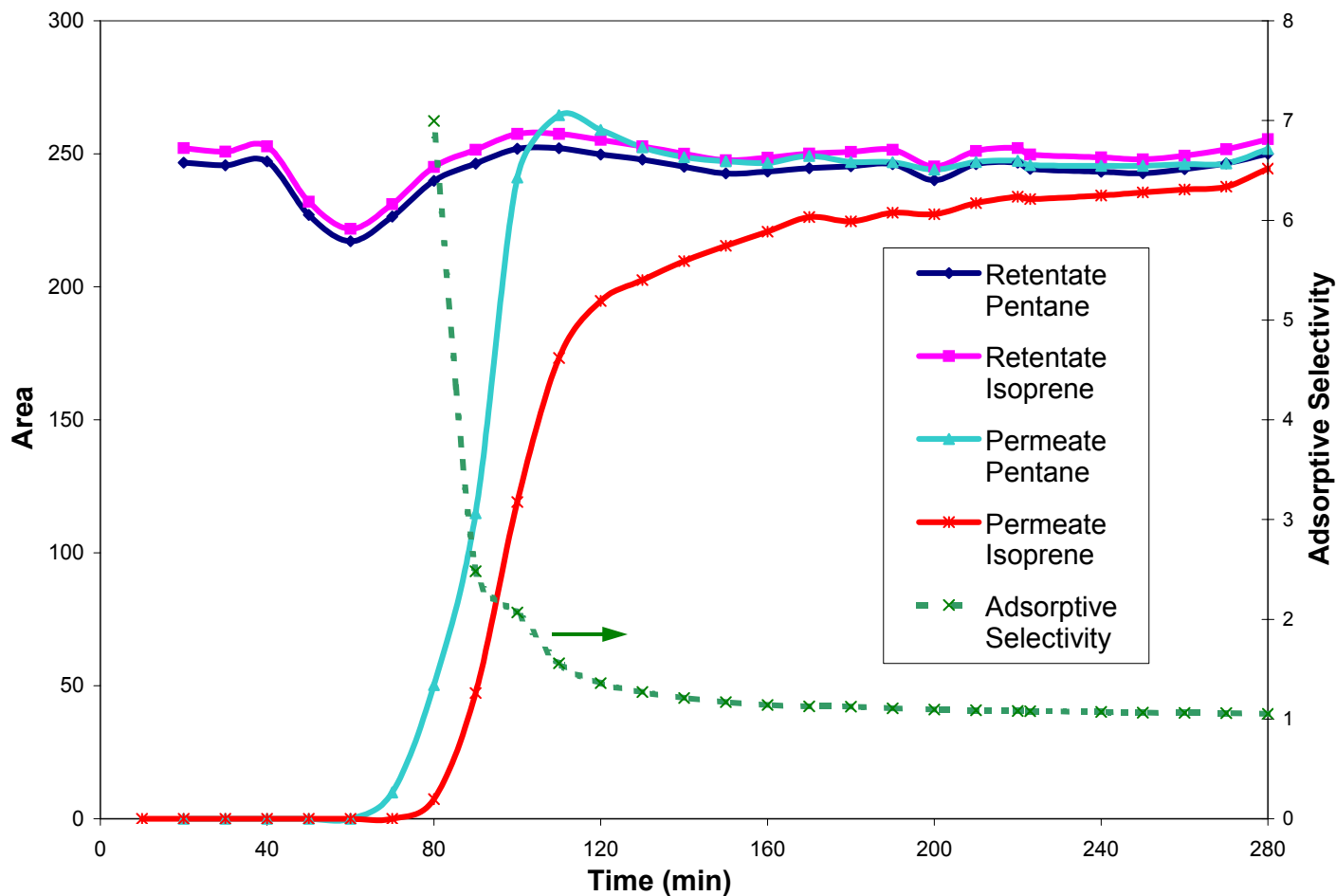
- *PXRD*
- *SEM*
- *pyridine-TPD*
- *BET*



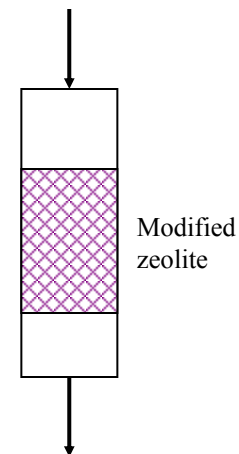
# Goodyear Separation Unit



# Experimental Results



Packed bed



Demonstrated isoprene/pentane separation using modified zeolite in dilute concentrations

Initial experiments show selectivity towards isoprene separation

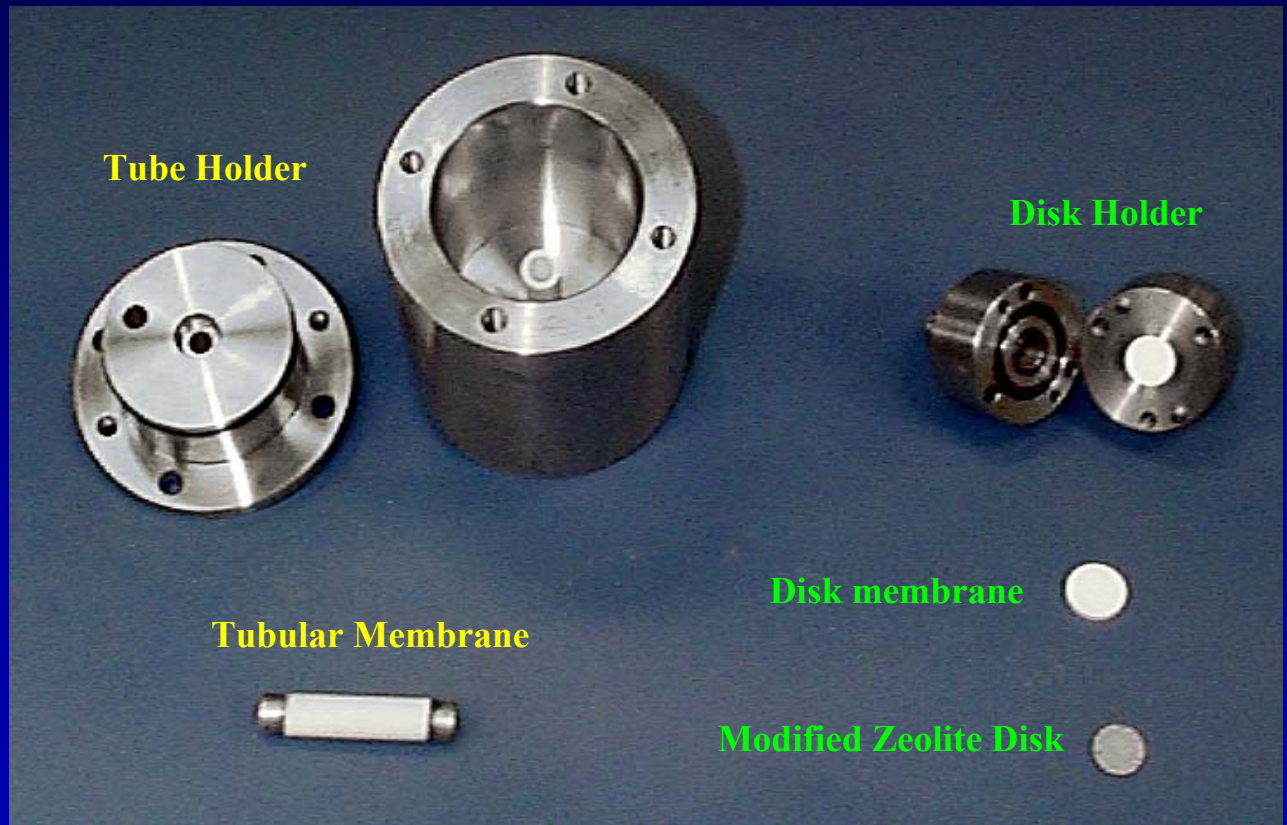
# — Technical Section:

## In-house Sandia Separation Unit

Test Unit



Test Cells

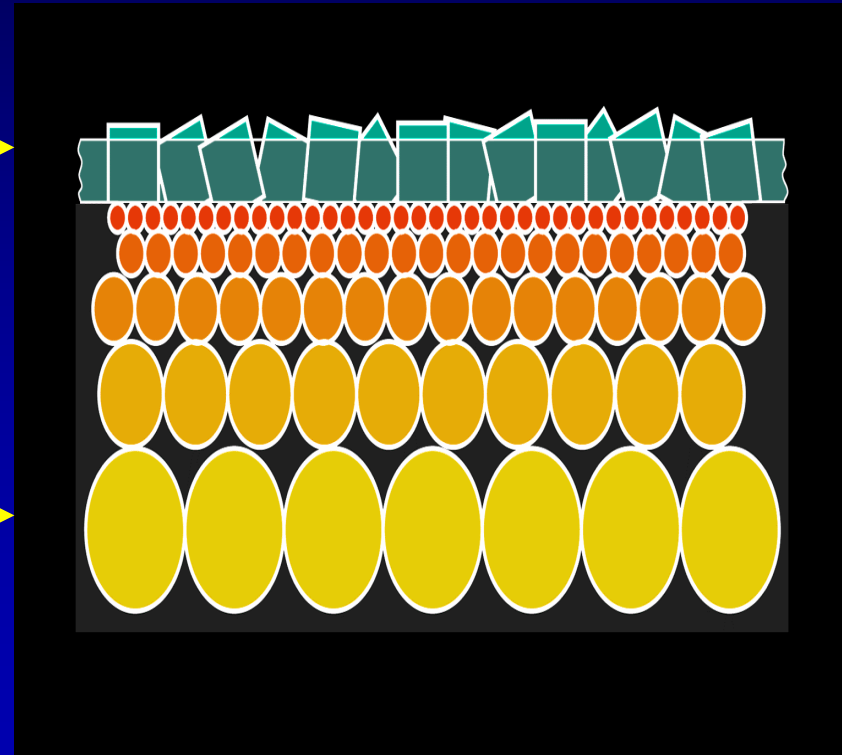
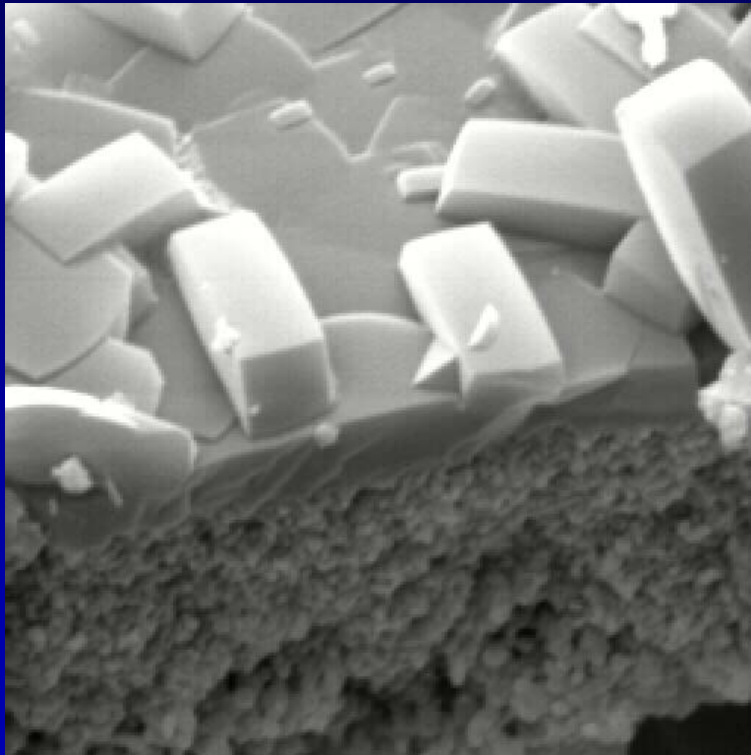




# — Technical Section : Membrane Development

- *Na-Y and Na-ZSM-5 membranes have been produced*
- *Surface modification of the supported membranes are under way*

Crystalline Zeolite Membrane Layer (Selectively allows only specified Molecules to pass through)

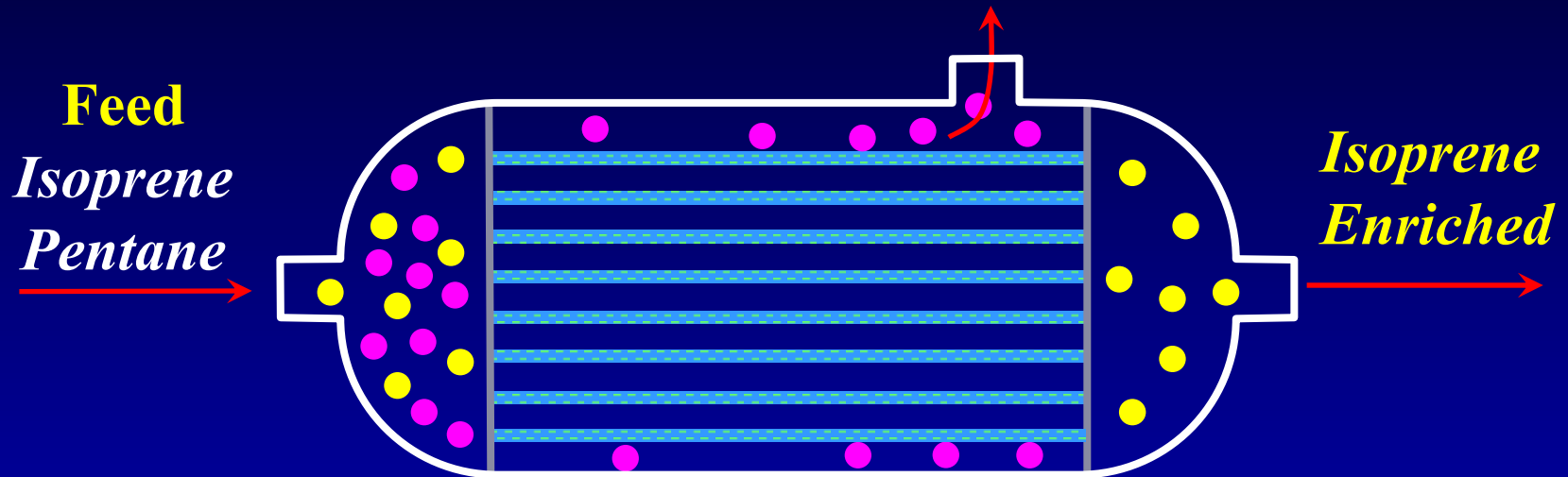


Support (allows all molecules to pass)

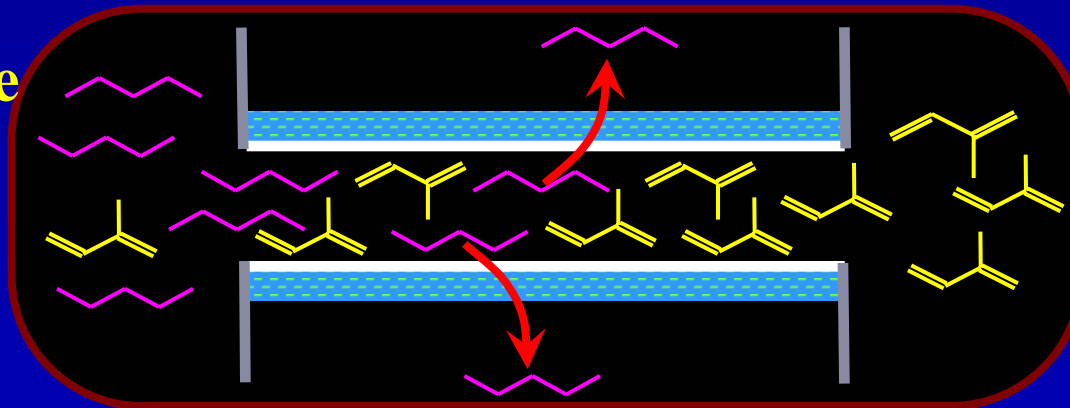


# — Technical Section: Possible Module Design

## *Enhanced Selectivity: Molecular Sieving + Adsorption*



- Pentane
- Isoprene



## — Summary : CRADA 1640.01 and IMF FY02

- Leveraged successful “Proof of Concept” FY01 in CRADA 1598 to a well funded winning DOE/OIT/IMF Proposal and New CRADA 1640.01
- DOE/OIT/IMF: Goodyear, Nofsinger, Sandia; \$1.2M for 3 years; *50% industry in-kind contributions*
- Economic feasibility studies completed; point to successful implementation of modified zeolites for HC separations
- Bulk modification and adsorption studies show enhancement for isoprene versus n-pentane using modified zeolites (Y).
- New work to further enhance the fundamental knowledge and skills for *isoprene purification* for bulk and membranes.





## — Acknowledgements

Sandia is a multiprogram laboratory operated by Sandia Corporation, a Lockheed Martin Company, for the US DOE under Contract DE-AC04-94-AL85000.

*Further Reading:*



OFFICE OF INDUSTRIAL TECHNOLOGIES



[http://www.oit.doe.gov/imf/factsheets/goodyr\\_zeolites.pdf](http://www.oit.doe.gov/imf/factsheets/goodyr_zeolites.pdf)



# Supplemental Energy Benefits from IMF Project

## Detailed Assumptions

- 22% Isoprene Energy Reduction
    - 1 % enrichment of isoprene which translates to 40,000,000 lbs. *LESS* raw materials processed to recover isoprene
  - 64 Trillion Btu/yr Savings for C2-C5 Industry
    - Obtained 1997 production and energy consumption for C2-C5 industries from *DOE/OIT Energy & Environmental Profile of the U.S. Chemical Industry* - May 2000
    - Calculated Btu's/lb based on 1997 numbers
    - Multiplied Btu's/lb (1997) by 2002 estimated billion lbs/yr (CMAI) to get current C2-C4 energy consumption by process
    - Ignored energy consumption by downstream processes
      - ex. polyethylene, polypropylene, SBR, etc.
-